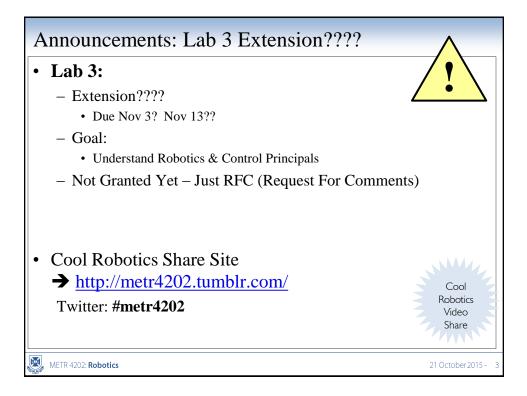
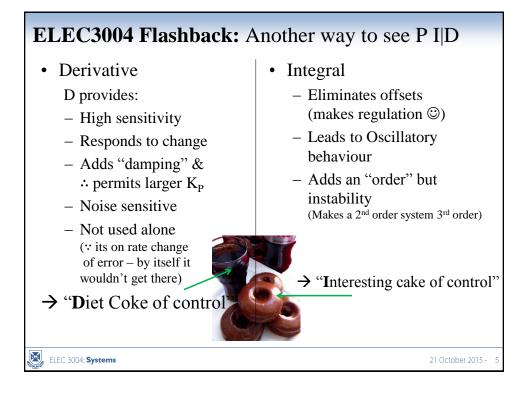
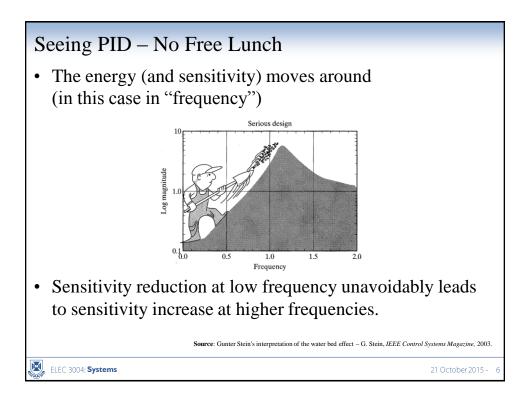


Schedule								
Week	Date	Lecture (W: 12:05-1:50, 50-N201)						
1	29-Jul	Introduction						
2		Representing Position & Orientation & State (Frames, Transformation Matrices & Affine Transformations)						
3	12-Aug	Robot Kinematics Review (& Ekka Day)						
4	19-Aug	Robot Dynamics						
5	26-Aug	Robot Sensing: Perception						
6	2-Sep	Robot Sensing: Multiple View Geometry						
7		Robot Sensing: Feature Detection (as Linear Observers)						
8	16-Sep	Probabilistic Robotics: Localization						
9	23-Sep	Quiz						
	30-Sep	Study break						
10	7-Oct	Motion Planning						
11	14-Oct	State-Space Modelling						
12	21-Oct	Shaping the Dynamic Response						
13	28-Oct	LQR + Course Review						
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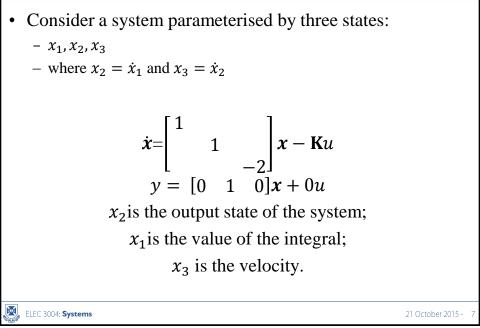


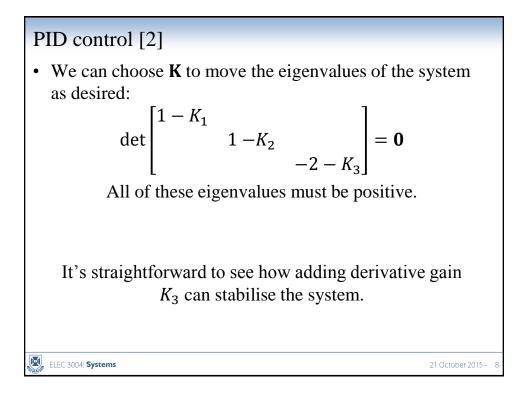
Shaping of Dynamic Responses





PID control





Implementation of Digital PID Controllers

We will consider the PID controller with an s-domain transfer function

$$\frac{U(s)}{X(s)} = G_c(s) = K_P + \frac{K_I}{s} + K_D s.$$
 (13.54)

We can determine a digital implementation of this controller by using a discrete approximation for the derivative and integration. For the time derivative, we use the **backward difference rule**

$$u(kT) = \frac{dx}{dt}\Big|_{t=kT} = \frac{1}{T}(x(kT) - x[(k-1)T]).$$
(13.55)

The z-transform of Equation (13.55) is then

$$U(z) = \frac{1 - z^{-1}}{T} X(z) = \frac{z - 1}{Tz} X(z).$$

The integration of x(t) can be represented by the **forward-rectangular integration** at t = kT as

$$u(kT) = u[(k-1)T] + Tx(kT), \qquad (13.56)$$

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Source: Dorf & Bishop, Modern Control Systems, §13.9, pp. 1030-1

Implementation of Digital PID Controllers (2) where u(kT) is the output of the integrator at t = kT. The z-transform of Equation (13.56) is $U(z) = z^{-1}U(z) + TX(z),$ and the transfer function is then $\frac{U(z)}{X(z)} = \frac{Tz}{z-1}.$ Hence, the z-domain transfer function of the **PID controller** is $G_c(z) = K_P + \frac{K_I T z}{z - 1} + K_D \frac{z - 1}{T z}.$ (13.57)The complete difference equation algorithm that provides the PID controller is obtained by adding the three terms to obtain [we use x(kT) = x(k)] $u(k) = K_P x(k) + K_I [u(k-1) + T x(k)] + (K_D/T) [x(k) - x(k-1)]$ $= [K_P + K_I T + (K_D/T)]x(k) - K_D T x(k-1) + K_I u(k-1).$ (13.58)Equation (13.58) can be implemented using a digital computer or microprocessor. Of course, we can obtain a PI or PD controller by setting an appropriate gain equal to zero. Source: Dorf & Bishop, Modern Control Systems, §13.9, pp. 1030-1 闽 ELEC 3004: Systems 21 October 2015 - 10

Let's Generalize This: Shaping the Dynamic Response • A method of designing a control system for a process in which all the state variables are accessible for Measurement → This method is also known as *pole-placement* Theory: • We will find that in a controllable system, with all the state variables accessible for measurement, it is possible to place the closed-loop poles anywhere we wish in the complex s plane! Practice: Unfortunately, however, what can be attained in principle may not be attainable in practice. Speeding the response of a sluggish system requires the use of large control signals which the actuator (or power supply) may not be capable of delivering. And, control system gains are very sensitive to the location of the open-loop poles METR 4202: Robotics 21 October 2015 - 11

Regulator Design

• Here the problem is to determine the gain matrix G in a linear feedback law $u = -Gx - G_0x_0$

- Where: x_0 is the vector of exogenous variables. The reason it is necessary to separate the exogenous variables from the process state x, rather than deal directly with the metastate $x = \begin{bmatrix} x \\ x_0 \end{bmatrix}$ is that we must assume that the underlying process is controllable.

• Since the exogenous variables are not true state variables, but additional inputs that cannot be affected by the control action, they cannot be included in the state vector when using a design method that requires controllability.

• HOWEVER, they can be used in a process for Observability! ∴ when we are doing this as part of the sensing/mapping process!!

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Regulator Design

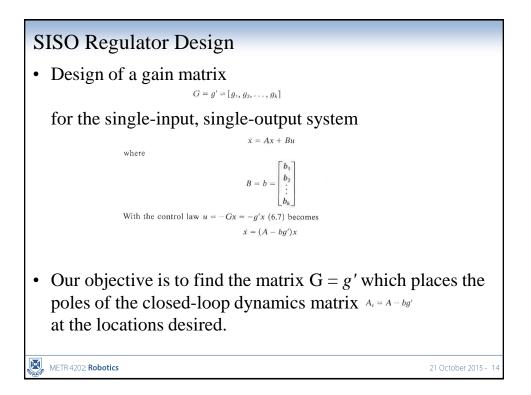
• The assumption that all the state variables are accessible to measurement in the regulator means that the gain matrix G in is permitted to be any function of the state **x** that the design method requires

y = Cx $u = -G_y y$ $u = -G\hat{x}$

– Where: \hat{x} is the state of an appropriate dynamic system known as an "observer."

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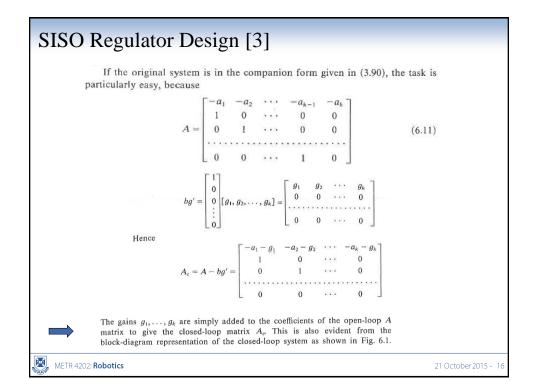
SISO Regulator Design [2]

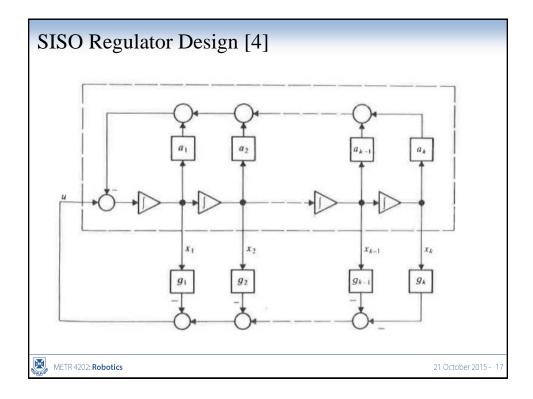
• One way of determining the gains would be to set up the characteristic polynomial for *Ac*:

 $|sI - A_c| = |sI - A + bg'| = s^k + \bar{a}_1 s^{k-1} + \dots + \bar{a}_k$

• The coefficients $a_1, a_2, ..., a_k$ of the powers of *s* in the characteristic polynomial will be functions of the *k* unknown gains. Equating these functions to the numerical values desired for $a_1, a_2, ..., a_k$ will result in *k* simultaneous equations the solution of which will yield the desired gains $g_1, ..., g_k$.

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SISO Regulator Design [4]						
• But how to get this in companion form?						
$ ilde{x} = Tx$	(6.14)					
Then, as shown in Chap. 3,						
$\dot{x} = \bar{A}\bar{x} + \bar{b}u$	(6.15)					
where $\bar{A} = TAT^{-1}$ and $\bar{b} = Tb$						
For the transformed system the gain matrix is						
$ar{g}=ar{a}-ar{a}=ar{a}-a$	(6.16)					
since $\bar{a} = a$ (the characteristic equation being invariant under a change of state variables). The desired control law in the original system is						
$u = -g'x = -g'T^{-1}\bar{x} = -\bar{g}'\bar{x}$	(6.17)					
From (6.17) we see that $\bar{g}' = g' T^{-1}$						
Thus the gain in the original system is						
$g = T' \bar{g} = T' (\hat{a} - a)$	(6.18)					
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SISO Regulator Design [5]

In words, the desired gain matrix for a general system is the difference between the coefficient vectors of the desired and actual characteristic equation, premultiplied by the inverse of the transpose of the matrix T that transforms the general system into the companion form of (3.90), the A matrix of which has the form (6.11).

The desired matrix T is obtained as the product of two matrices U and V:

$$T = VU \tag{6.19}$$

The first of these matrices transforms the original system into an intermediate system

$$\dot{\tilde{x}} = \tilde{A}\tilde{x} \tag{6.20}$$

in the second companion form (3.107) and the second transformation U transforms the intermediate system into the first companion form.

Consider the intermediate system

$$\dot{\tilde{x}} = \tilde{A}\tilde{x} + \tilde{b}u \tag{6.21}$$

(6.22)

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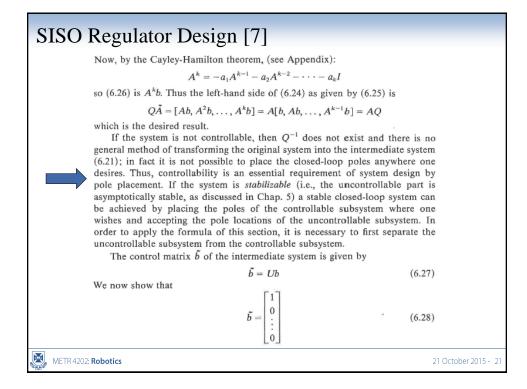
with \tilde{A} and \tilde{b} in the form of (3.107). Then we must have

$$\tilde{A} = UAU^{-1}$$
 and $\tilde{b} = Ub$

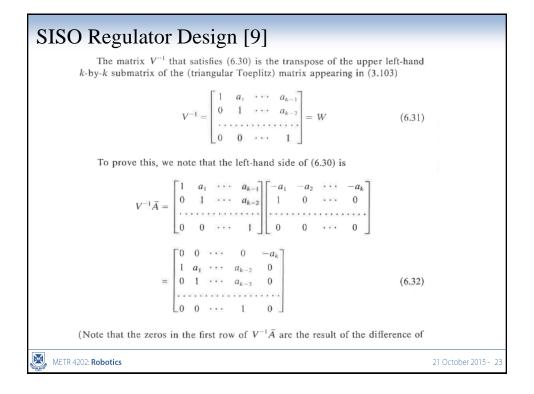
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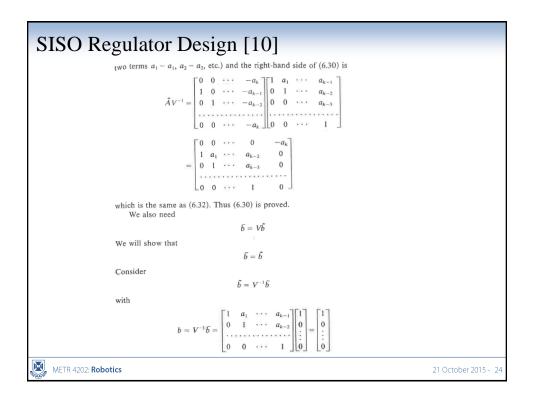
SISO Regulator Design [6] The desired matrix U is precisely the inverse of the controllability test matrix Q of Sec. 5.4. To prove this fact, we must show that $U^{-1}\tilde{A} = AU^{-1}$ (6.23)or $O\tilde{A} = AQ$ (6.24)Now, for a single-input system $Q = [b, Ab, \dots, A^{k-1}b]$ Thus, with \tilde{A} given by (3.107), the left-hand side of (6.23) is $0 \quad 0 \quad \cdots \quad -a_k$ $Q\tilde{A} = [b, Ab, \dots, A^{k-1}b] \begin{bmatrix} 0 & 0 & \cdots & -a_{k-1} \\ 1 & 0 & \cdots & -a_{k-1} \\ 0 & 1 & \cdots & -a_{k-2} \\ \cdots & \cdots & \cdots & \cdots \\ 0 & 0 & \cdots & -a_{1} \end{bmatrix}$ = $[Ab, A^2b, \ldots, A^{k-1}b, -a_kb - a_{k-1}Ab - \cdots - a_kA^{k-1}b]$ (6.25)The last term in (6.25) is $(-a_kI - a_{k-1}A - \cdots - a_kA^{k-1})b$ (6.26)X METR 4202: Robotics 21 October 2015 - 20

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SISO Regulator Design [8] Multiply (6.28) by Q to obtain $Q\tilde{b} = [b, Ab, \dots, A^{k-1}b] \begin{bmatrix} 1\\0\\\vdots\\0 \end{bmatrix} = b$ which is the same as (6.27), since $Q^{-1} = U$. The final step is to find the matrix V that transforms the intermediate system (6.21) into the final system (6.15). We must have $\bar{x} = V\tilde{x}$ (6.29)For the transformation (6.28) to hold, we must have $\bar{A} = V \tilde{A} V^{-1}$ or $V^{-1}\vec{A} = \tilde{A}V^{-1}$ (6.30)× METR 4202: Robotics 21 October 2015 -





SISO Regulator Design [11]

Thus \tilde{b} and \bar{b} are the same.

The result of this calculation is that the transformation matrix T whose transpose is needed in (6.18) is the inverse of the product of the controllability test matrix and the triangular matrix (6.31).

The above results may be summarized as follows. The desired gain matrix g, by (6.18) and (6.19), is given by

$$g = (VU)'(\hat{a} - a)$$
 (6.33)

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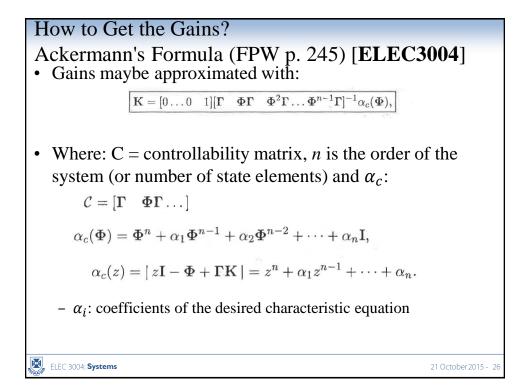
where

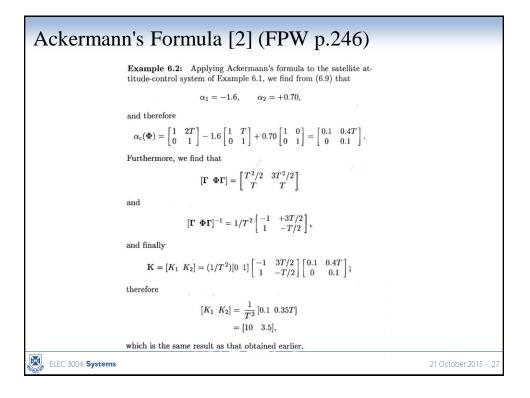
 $V = W^{-1} \qquad \text{and} \qquad U = Q^{-1}$

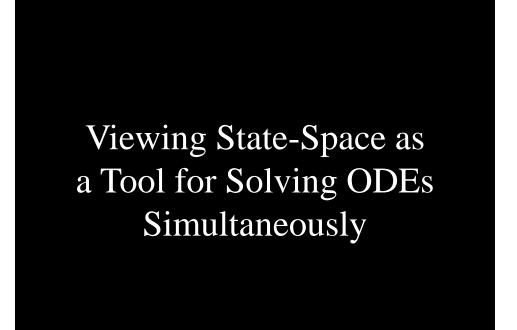
Thus

$$VU = W^{-1}Q^{-1} = (QW)^{-1}$$

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State Space as an ODE

• The basic mathematical model for an LTI system consists of the state differential equation

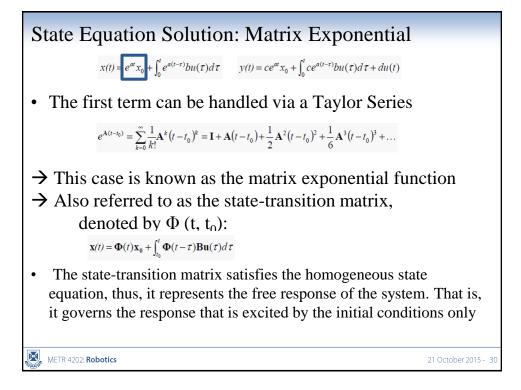
```
\dot{\mathbf{x}}(t) = \mathbf{A}\mathbf{x}(t) + \mathbf{B}\mathbf{u}(t) \qquad \mathbf{x}(t_0) = \mathbf{x}_0\mathbf{y}(t) = \mathbf{C}\mathbf{x}(t) + \mathbf{D}\mathbf{u}(t)
```

• The solution is can be expressed as a sum of terms owing to the initial state and to the input respectively:

 $x(t) = e^{at}x_0 + \int_0^t e^{a(t-\tau)}bu(\tau)d\tau \qquad y(t) = ce^{at}x_0 + \int_0^t ce^{a(t-\tau)}bu(\tau)d\tau + du(t)$ zero-input response zero-state response

• This is a first-order solution similar to what we expect

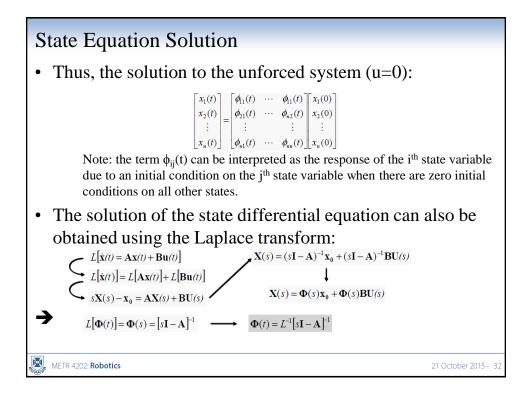
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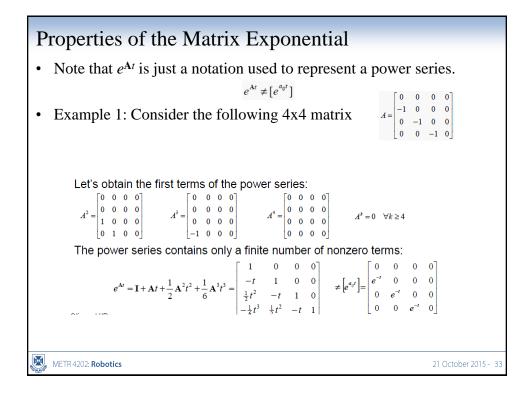


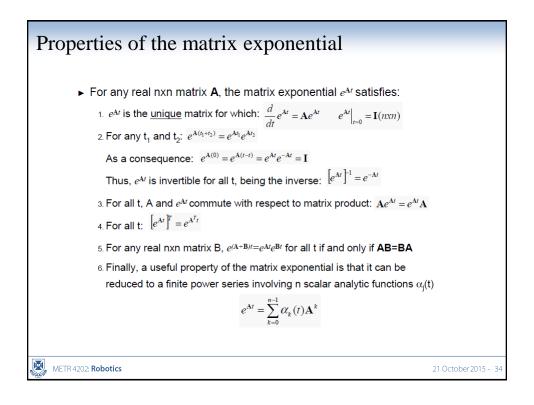
Output Equation Solution

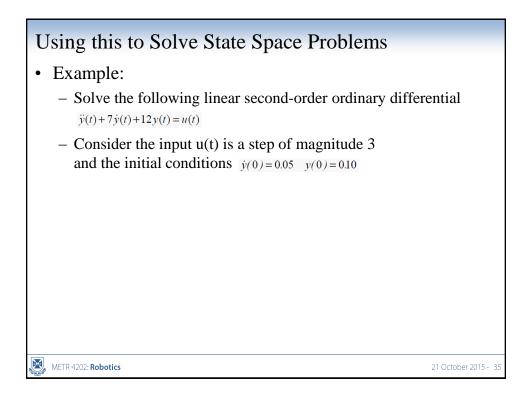
• Having the solution for the complete state response, a solution for the complete output equation can be obtained as:

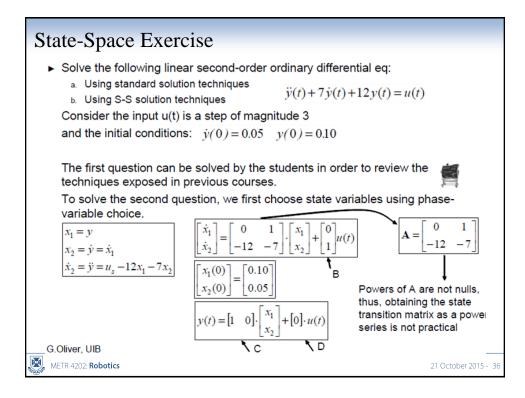
	$\mathbf{y}(t) = \mathbf{C}e^{\mathbf{A}t}\mathbf{x}_0 + \int_{t_0}^t \mathbf{C}e^{\mathbf{A}t}$		
zero-input re	esponse: y _{zi} (t)	y _{zs} (t): zero-state response	
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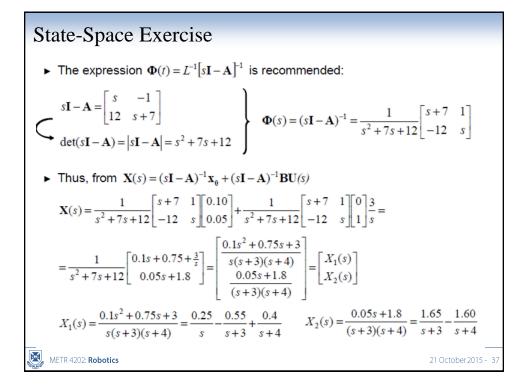


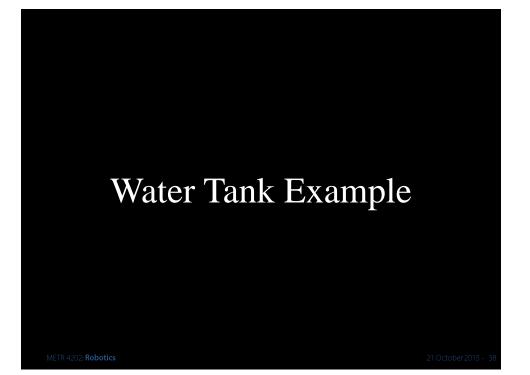


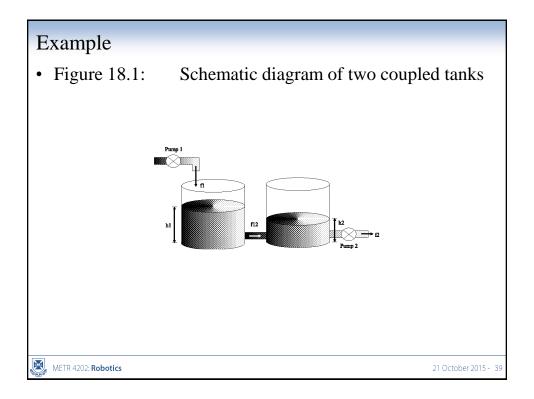


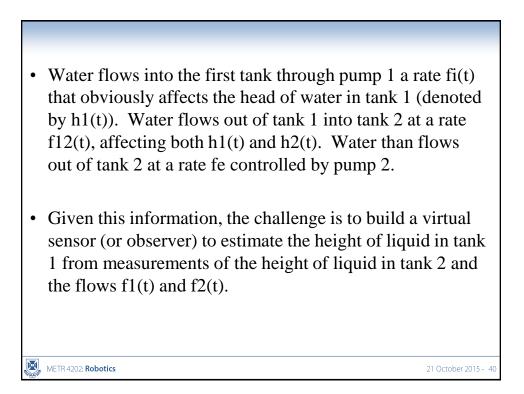












• Before we continue with the observer design, we first make a model of the system. The height of liquid in tank 1 can be described by the equation

$$\frac{dh_1(t)}{dt} = \frac{1}{A}(f_i(t) - f_{12}(t))$$

• Similarly, h2(t) is described by

$$rac{dh_2(t)}{dt} = rac{1}{A}(f_{12}(t) - f_e)$$

• The flow between the two tanks can be approximated by the free-fall velocity for the difference in height between the two tanks:

$$f_{12}(t) = \sqrt{2g(h_1(t) - h_2(t))}$$

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- We can linearize this model for a nominal steady-state height difference (or operating point). Let
- This yields the following linear model:

$$h_1(t) - h_2(t) = \Delta h(t) = H + h_d(t)$$

• where

$$\frac{d}{dt} \begin{bmatrix} h_1(t) \\ h_2(t) \end{bmatrix} = \begin{bmatrix} -k & k \\ k & -k \end{bmatrix} \begin{bmatrix} h_1(t) \\ h_2(t) \end{bmatrix} + \begin{bmatrix} 1 & 0 \\ 0 & -1 \end{bmatrix} \begin{bmatrix} f_1(t) - \frac{K\sqrt{H}}{2} \\ f_2(t) + \frac{K\sqrt{H}}{2} \end{bmatrix}$$

$$k = \frac{K}{2\sqrt{H}}$$

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• We are assuming that h2(t) can be measured and h1(t) cannot, so we set C = [0 1] and D = [0 0]. The resulting system is both controllable and observable (as you can easily verify). Now we wish to design an observer

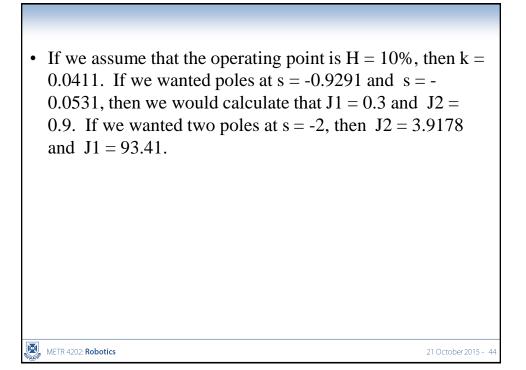
$$J = egin{bmatrix} J_1 \ J_2 \end{bmatrix}$$

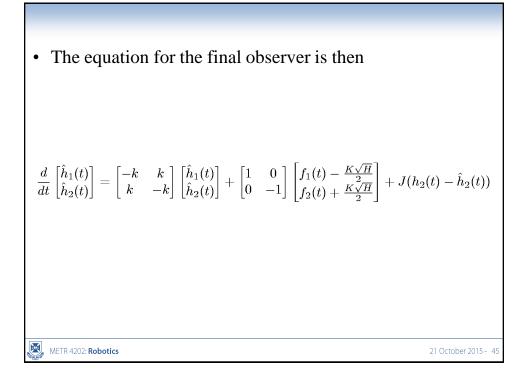
• to estimate the value of h2(t). The characteristic polynomial of the observer is readily seen to be

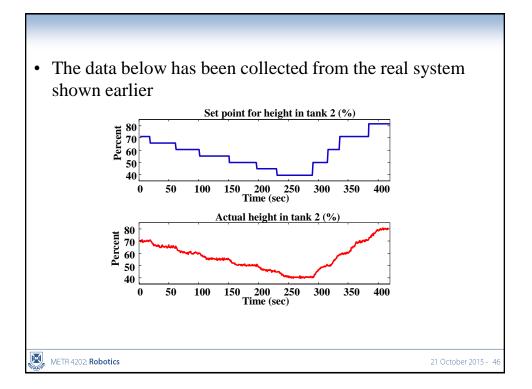
 $s^2 + (2k + J_1)s + J_2k + J_1k$

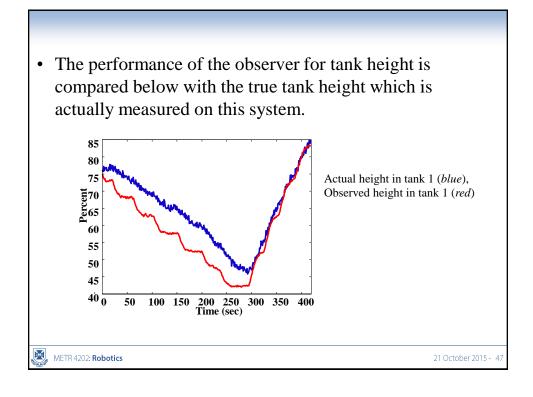
• so we can choose the observer poles; that choice gives us values for J1 and J2.

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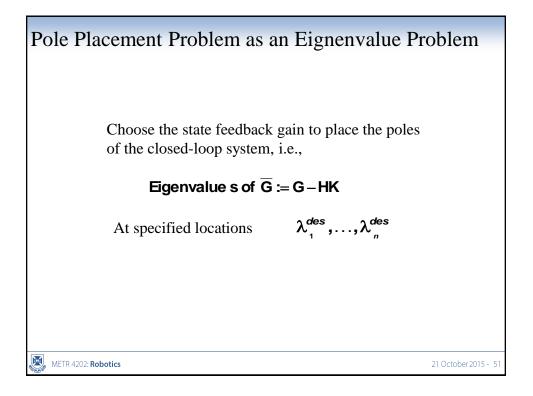
Pole Assignment by State Feedback

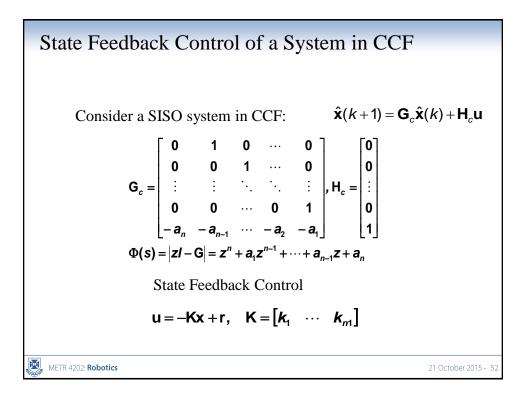
• We begin by examining the problem of closed-loop pole assignment. For the moment, we make a simplifying assumption that all of the system states are measured. We will remove this assumption later. We will also assume that the system is completely controllable. The following result then shows that the closed-loop poles of the system can be arbitrarily assigned by feeding back the state through a suitably chosen constant-gain vector.

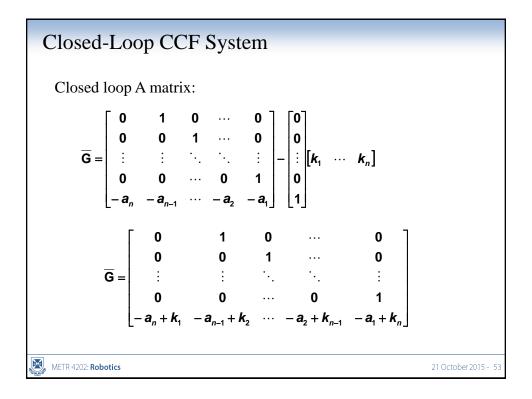
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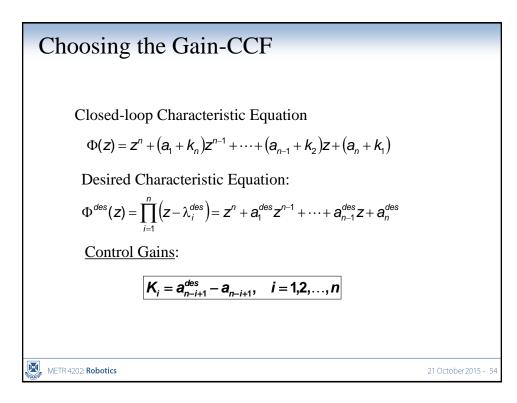
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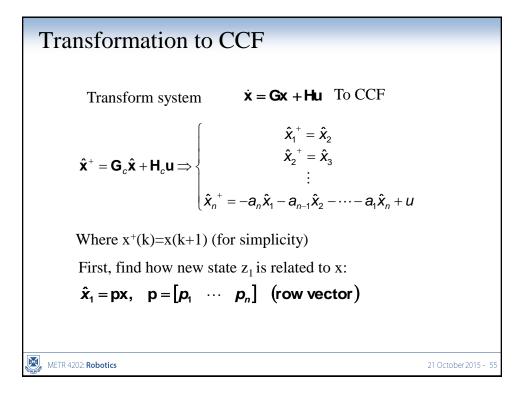
State-Feedback Control Objectives
Regulation: Force state x to equilibrium state (usually 0) with a desirable dynamic response.
Tracking: Force the output of the system y to tracks a given desired output y_d with a desirable dynamic response.

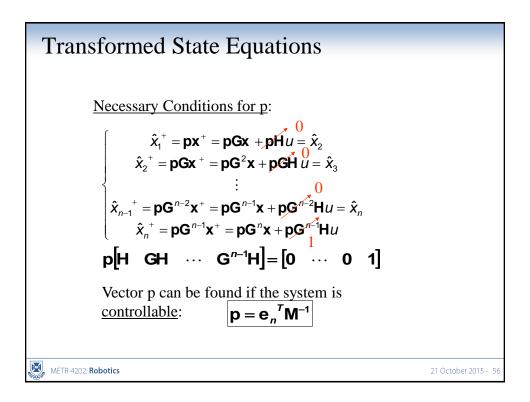


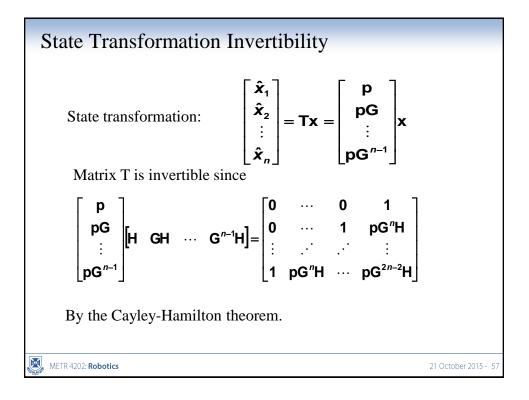


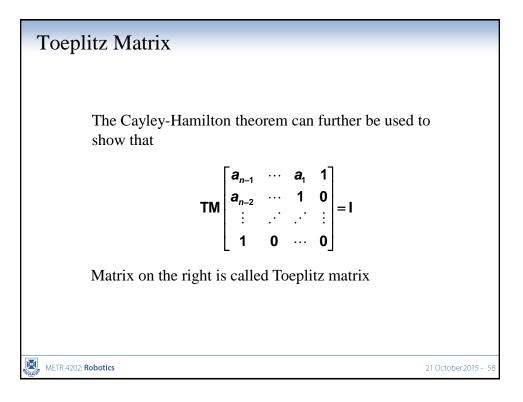


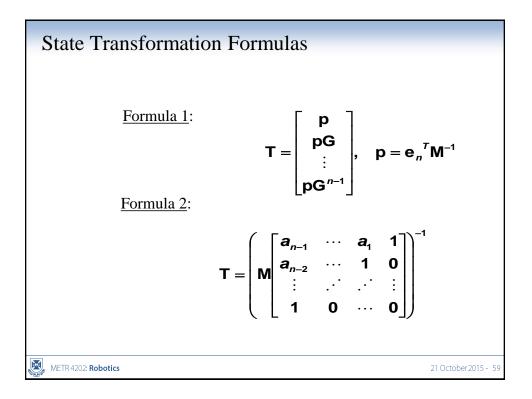


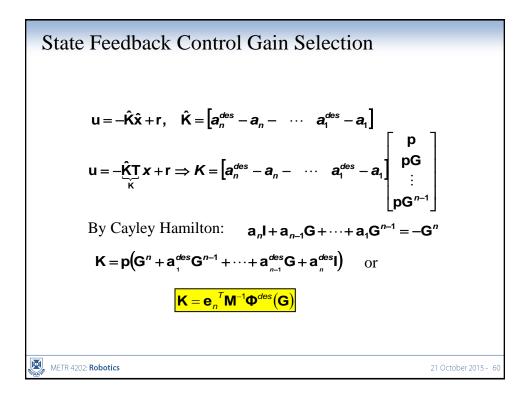


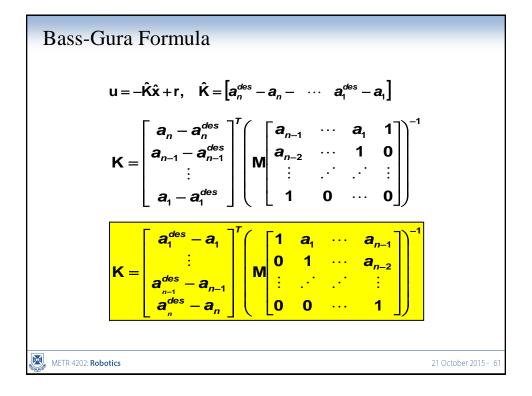


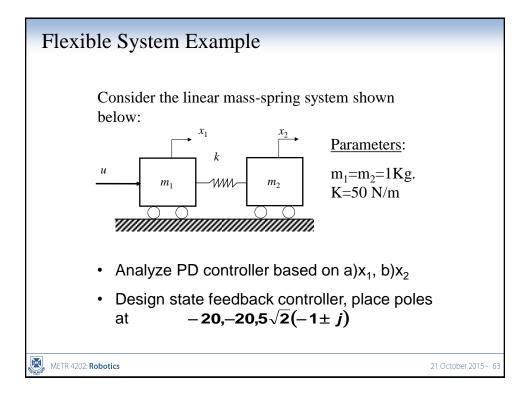


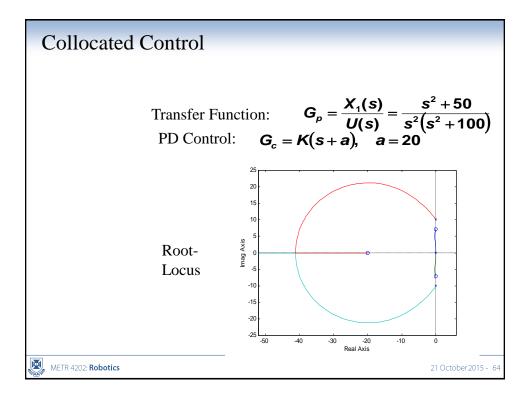


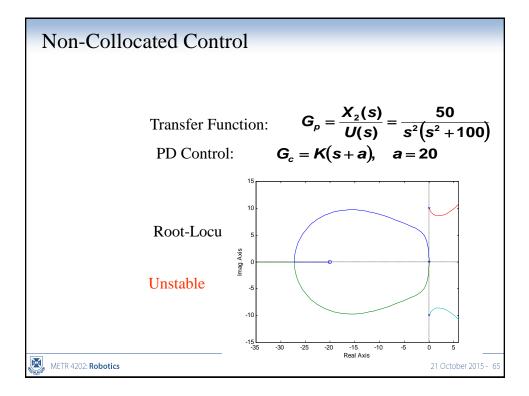


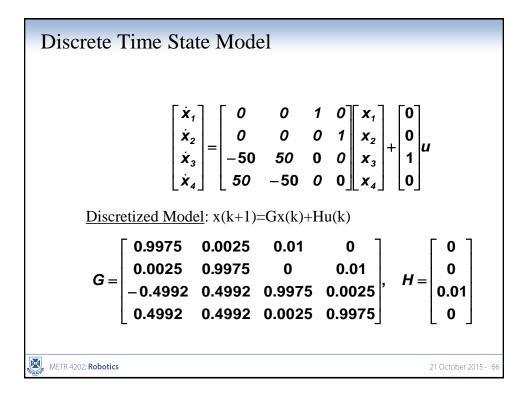


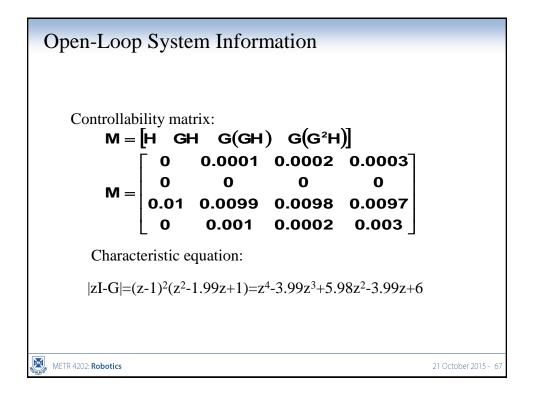


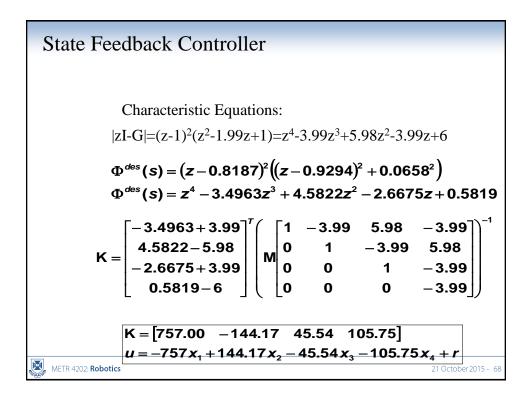










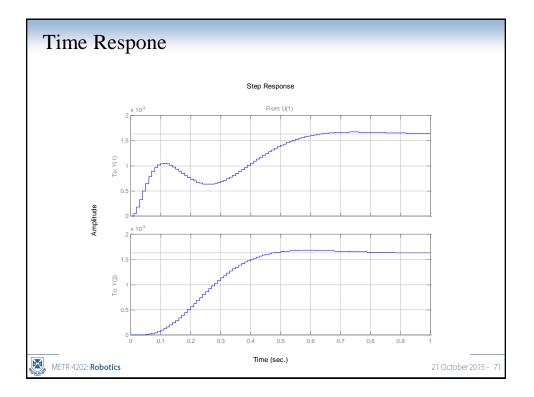


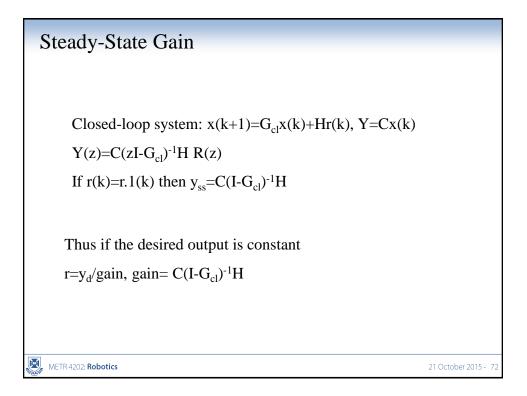
Matlab Solution

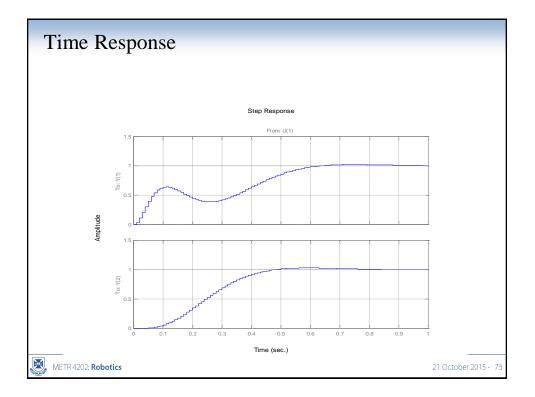
```
%System Matrices
m1=1; m2=1; k=50; T=0.01;
syst=ss(A,B,C,D);
A=[0 0 1 0;0 0 0 1;-50 50 0 0;50 -50 0 0];
B=[0; 0; 1; 0];
C=[1 0 0 0;0 1 0 0]; D=zeros(2,1);
cplant=ss(A,B,C,D);
%Discrete-Time Plant
plant=c2d(cplant,T);
[G,H,C,D]=ssdata(plant);
```

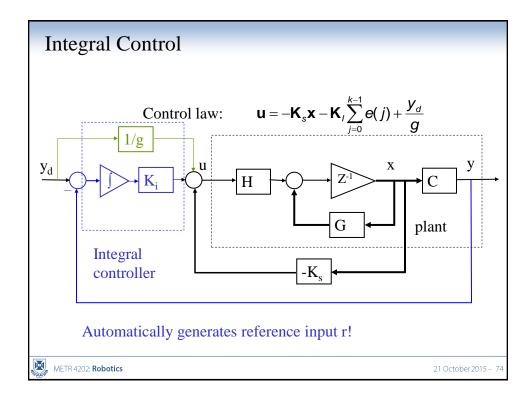
METR 4202: Robotics

```
Matlab Solution
%Desired Close-Loop Poles
pc=[-20;-20;
    -5*sqrt(2)*(1+j); 5*sqrt(2)*(1-j)];
pd=exp(T*pc);
% State Feedback Controller
K=acker(G,H,pd);
%Closed-Loop System
clsys=ss(G-H*K,H,C,0,T);
grid
step(clsys,1)
```

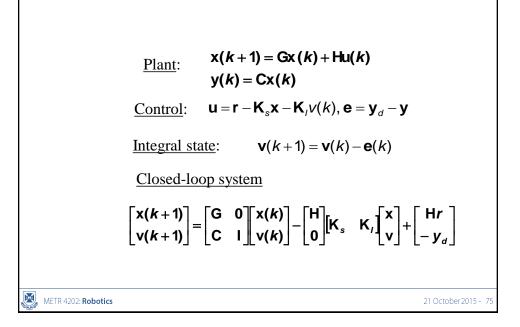








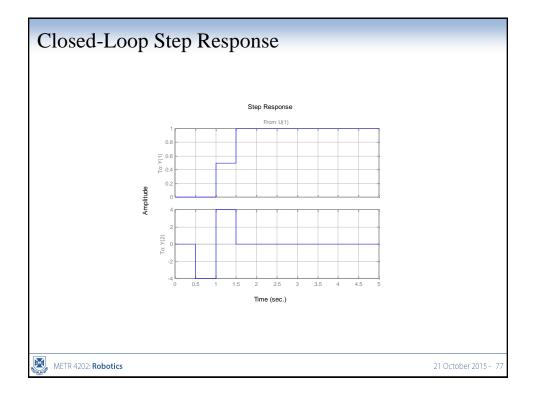


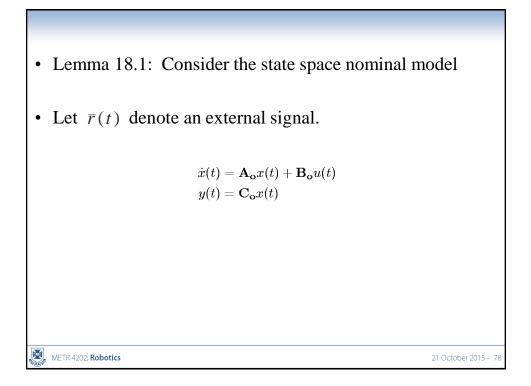


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Double Integrator-Matlab Solution

F=0.5;
lam=[0;0;0];
G=[1 T;0 1]; H=[T^2/2;T]; C=[1 0];

Gbar=[G zeros(2,1);C 1];
Hbar=[H;0];
K=acker(Gbar,Hbar,lam);
Gcl=Gbar-Hbar*K;
yd=1; r=0; %unknown gain
clsys=ss(Gcl,[H*r;-yd],[C 0;K],0,T);
step(clsys);
```





• Then, provided that the pair (A0, B0) is completely controllable, there exists

 $egin{aligned} u(t) &= ar{r} - \mathbf{K} x(t) \ \mathbf{K} \stackrel{ riangle}{=} [k_0, k_1, \dots, k_{n-1}] \end{aligned}$

• such that the closed-loop characteristic polynomial is $A_{cl}(s)$, where $A_{cl}(s)$ is an arbitrary polynomial of degree n.

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Note that state feedback does not introduce additional dynamics in the loop, because the scheme is based only on proportional feedback of certain system variables. We can easily determine the overall transfer function from *r*(*t*) to y(t). It is given by ^{Y(s)}/_{*R*(s)} = C_o(sI − A_o + B_oK)⁻¹B_o = C_oAdj{sI − A_o + B_oK}B_o/*F*(s)

where

 F(s) [△]/_e det{sI − A_o + B_oK}

and Adj stands for adjoint matrices.

[Matrix inversion lemma]

- We can further simplify the expression given above. To do this, we will need to use the following results from Linear Algebra.
- (Matrix inversion lemma). Consider three matrices A,B,C Then, if A + BC is nonsingular, we have that (A + BC)⁻¹ = A⁻¹ - A⁻¹B (I + CA⁻¹B)⁻¹CA⁻¹
 In the case for which B = g ∈ In and CT = h ∈ In, the
- above result becomes $f(x) = g \in [0, 1]$ and C = f(x) = f(x)

$$\left(\mathbf{A}+gh^T
ight)^{-1}=\left(\mathbf{I}-\mathbf{A}^{-1}rac{gh^T}{1+h^T\mathbf{A}^{-1}g}
ight)\mathbf{A}^{-1}$$

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• Lemma 18.3: Given a matrix $W \in \squaren \times n$ and a pair of arbitrary vectors $\phi 1 \in \squaren$ and $\phi 2 \in \squaren$, then provided that W and are nonsingular,

$$W+\phi_1\phi_2^T$$
,

• Proof: See the book.

 $egin{aligned} Adj(W+\phi_1\phi_2^T)\phi_1 &= Adj(W)\phi_1 \ \phi_2^TAdj(W+\phi_1\phi_2^T) &= \phi_2^TAdj(W) \end{aligned}$

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